

ASSESSING THE OPENFOAM INTERFOAM SOLVER BY NUMERICAL MODELLING THE EXTENSIONAL FLOW TEST

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Introduction

- Rheology plays an essential role in the analysis and optimization of polymer processing. As happens in many areas, those activities clearly benefit from the support of computational tools.
- In polymer processing, multi-phase flows comprise several challenging computational problems, that would benefit from accurate modeling codes.
- The interFoam solver, from OpenFOAM computational library, allows to model multiphase flows, with a robust Volume of Fluid approach.

Objectives

- Model the extensional rheometry test, based on the Sentmanat Extensional Rheometer (SER) platform.
- Assess of the interFoam solver, in the framework of polymer processing applications, by comparing its predictions with data collected in experimental measurements.

Material & Methods

- The maximum Courant number of $1e-4$ is used for all the case studies.
- The number of the mesh cells used for the first geometry (G1) is 79947 and it is 26790 for the second one (G2).
- G2 was proposed to solve problems identified with G1. Applied boundary conditions in G2 avoid the air penetration into the polymer-cylinder interface (PCI).
- Two discretization schemes with different orders (Upwind – first-order interpolation method and MINMOD – second order interpolation method) was used for the advection term.

Discussion

- As shown in (P1), with Upwind the value of numerical diffusion at the free-surface is higher, and it was significantly reduced when using MINMOD for the advection terms (P2).
- Mesh refinement leads to the reduction of air penetration (P3 vs P4), but it remains. While the mentioned phenomenon totally solved with G2 (P5).
- Indeed, the air penetration phenomenon promotes a significant difference between the applied velocity onto the cylinder and the velocity on the surface of the polymer. This leads to a huge error (25%) in the velocity gradient imposed on the polymeric sample (Graph1).
- The worse mesh from G1 promotes unstable calculations, which requires a long computational time.
- The velocity gradient of the numerical modelling is in very good agreement with the theoretical one, and the error reduced considerably ($\leq 4\%$) (Graph2). A small difference between the numerical data and the theoretical one, visible at the beginning of the calculation (Graph1), is promoted by the sample inertia, which also happens in practice.
- On the other hand, the mesh non-orthogonality was substantially reduced (from 44.44 to 0.57) with G2.
- The calculation time decreased from 17 hours for G1 to 14 hours in G2.

Conclusion

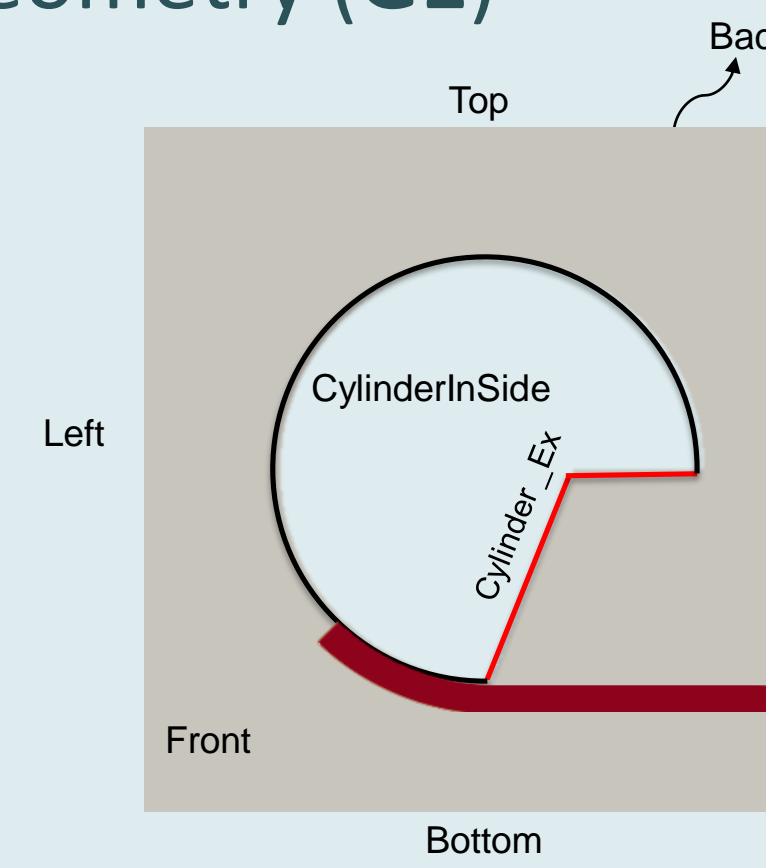
- This work allowed to identify the appropriate calculation framework to perform the envisaged assessment studies.
- The discretization scheme (Upwind and MINMOD, etc.) for the advection terms plays an essential role in the numerical diffusion reduction.
- Achieving results with higher accuracy requires to use of appropriate geometry and boundary conditions.

Acknowledgements

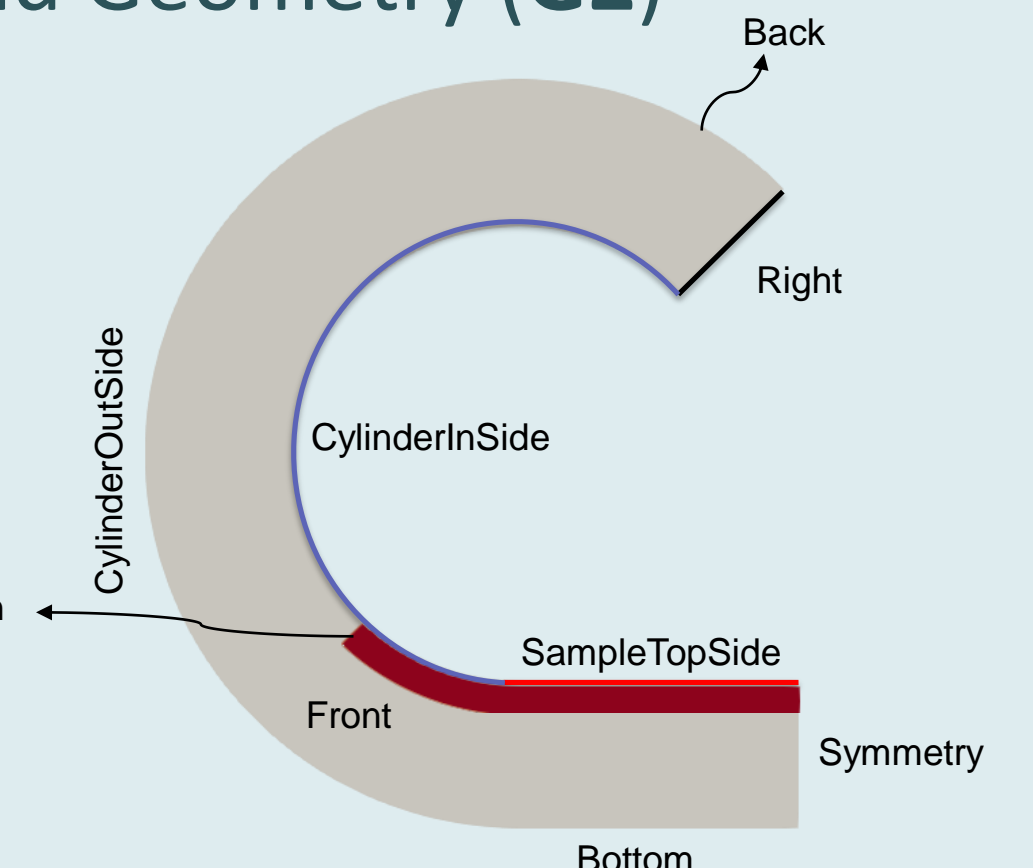
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Geometries & Boundary Conditions

First Geometry (G1)



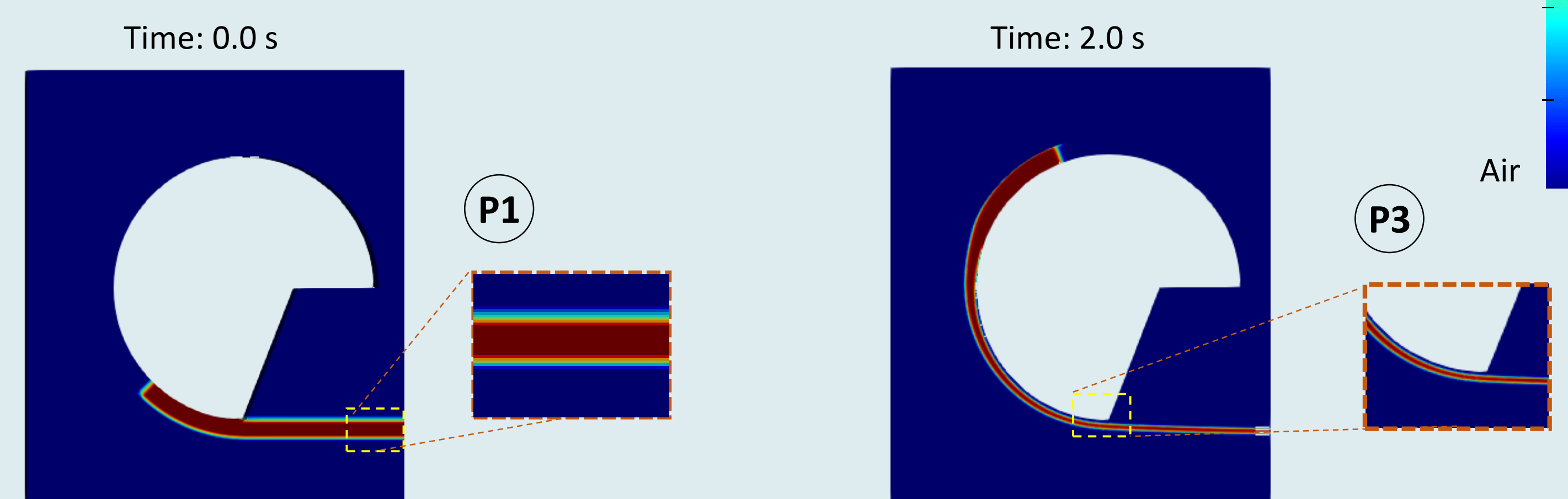
Second Geometry (G2)



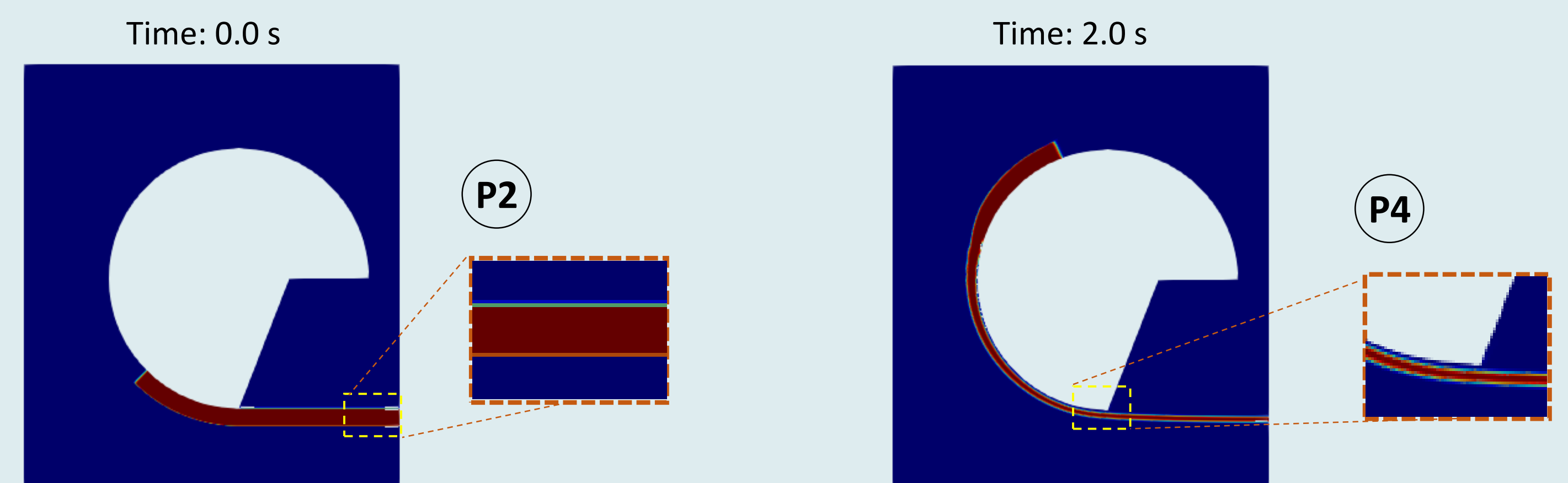
Boundary Condition (2D Case)				
Geometry type	Faces/Sides	Velocity file	Pressure file	Alpha file
G1 + G2	CylinderInSide	Rotating Velocity (1 radian/s)	null normal gradient	null normal gradient
G1	Cylinder_Ext	null normal gradient	null normal gradient	null normal gradient
G1	Top & Left	null normal gradient	null normal gradient	null normal gradient
G1 + G2	Bottom	null normal gradient	null normal gradient	null normal gradient
G2	CylinderOutSide	null normal gradient	null normal gradient	null normal gradient
G2	SampleTopSide	Full slip	null normal gradient	Uniform value (1)
G2	Right	null normal gradient	Uniform value (1 Pa)	null normal gradient

Results

G1: Upwind Scheme



G1: MINMOD Scheme



G2: MINMOD Scheme

